

TITLE OF THE INVENTION

HIGH-STRUCTURE PRECIPITATED SILICAS

BACKGROUND OF THE INVENTION

Field of the Invention

The present invention relates to precipitated silicas having a high structure, to a process for the manufacture of the silicas and to the use of these silicas.

Description of the Background

The structure of a silica is understood to be the extent to which its primary particles congregate into secondary particles or, respectively, tertiary particles. The unit used to express the size of the structure is the Brabender dibutyl phthalate (DBP) absorption coefficient.

Spray dried precipitated silicas are known and sold, for instance, under the brand name of Sipernat®. The silicas are usually manufactured by precipitating water glass with sulfuric acid, wherein the entire width of possible precipitation variants can be deployed, as described, for example in EP 0 078 909, U.S. Patent 4,094,771 or U.S. Patent 6,013,234.

After precipitation the solid matter is removed by filtration and the filter cake is then spray-dried. If necessary, it is re-dispersed by adding an acid. Spray drying allows the manufacture of almost spherical, solid particles with a narrow size distribution range.

Silicas with DBP absorption values of up to 380 g/110 g are known as described in EP 0 078 909. In Example 1 of the present application, a silica with 380 g/100 g DBP absorption

value is obtained by spray-drying a silica suspension containing 11% solids by weight. According to Example 5 of the present application a DBP absorption of 346 g/100 g is obtained by spray-drying a silica suspension containing 16% solid matter by weight.

A similar process is disclosed in U.S. Patent 6,013,234. In this case a silica suspension with pH > 4 and a solids content of more than 18% by weight was spray-dried to form particles with an average particle diameter of more than 150 μm and a BET surface area of 100 to 350 m^2/g .

The known spray dried precipitated silicas can be improved with respect to their DBP absorption values.

SUMMARY OF THE INVENTION

Accordingly, one object of the present invention is to provide silicas of improved physical characteristics.

Briefly, this object and other objects of the present invention as hereinafter will become more readily apparent can be attained by precipitated silicas having the following physico-chemical data:

pH (5% in water) (ISO 787-9)		3 - 8
BET surface area (DIN 66131)	(m^2/g)	400 - 600
DBP absorption value (DIN 53601, in relation to dried substance)	(g/100 g)	380 - 420
Tapped density (ISO 787-11)	(g/l)	100 - 200
ALPINE sieve residue > 63 μ (ISO 8130-1)	(%)	0.1 - 40

DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

Surprisingly, it has now been discovered that high-structured spray-dried silicas with DBP absorption values of more than 380 g/100 g can be obtained by employing a specific precipitation method.

Precipitated silicas of variant I of the present invention have the following physico-chemical characteristics.

Variant	II	III	IV
pH (5% in water) (ISO 787-9)	3 - 8	3 - 8	3 - 8
BET surface area (DIN 66131) (m ² /g)	400 - 600	400 - 600	400 - 600
DBP absorption value (DIN 53601, in relation to dried substance) (g/100 g)	380 - 420	380 - 420	380 - 420
Tapped density (ISO 787-11) (g/l)	140 - 200	120 - 180	100 - 130
ALPINE sieve residue > 63μ (ISO 8130-1) (%)	10 - 40	1 - 10	0,1 - 1

Another variant of the precipitated silicas of the present invention have the following physico-chemical characteristics:

Variant	I	II	III	IV
pH (5% in water) (ISO 787-9)	3 - 8	3 - 8	3 - 8	3 - 8
BET surface area (DIN 66131) (m ² /g)	400 - 600	400 - 600	400 - 600	400 - 600
DBP absorption value (DIN 53601, in relation to dried substance) (g/100 g)	380 - 420	380 - 420	380 - 420	380 - 420
Tapped density (ISO 787-11) (g/l)	100 - 200	140 - 200	120 - 180	100 - 130
ALPINE sieve residue > 63μ (ISO 8130-1) (%)	0.1 - 40	10 - 40	1 - 10	0.1 - 1

The variants of silica of the present invention can be prepared by a process in which,

while stirring water in a vessel with a force sufficient to subject the medium to shear while the water is heated to 35°C to 45°C, water and sulfuric acid are added together to the medium within at least 100 minutes. The pH is maintained at 6–7. The introduction of substances into the vessel is then interrupted for 60–120 minutes and when the addition of the substances has been completed, the medium contains a solids content of 36–42 g/l. The solids are removed by filtration, the filter cake is washed and the solid material is subjected to a short retention drying process

A special variant of the process is such that while stirring a vessel containing water heated to 35°C to 45°C, preferably 36°C to 40°C and maintaining a pH of 6–7 and adding waterglass and sulfuric acid together, while the mixture is subjected to shear during the entire precipitation time with a disk agitator installed in addition to the agitator, by interrupting the precipitation for 90 minutes from the 13th to the 103rd minute, after a total precipitation time of 137 minutes, a final silica concentration of 38 to 42 g/l is established in the precipitation suspension. The precipitation suspension is then filtered and washed, the filter cake is dried or liquefied by adding water and/or acid to form a suspension containing 8% to 16% solid matter. The suspension is then spray-dried.

The short retention time drying in process stage c) can be conducted by liquefying the filter cake to a solids content of less than 18% by weight and spray-drying the suspension.

In another variant of the process of the present invention the short retention time drying process can be conducted by means of a spin-flash drying process on the washed filter cake from process stage b).

The pH of the end product is of decisive importance for many applications of the silicas. For instance, if the silica is used as a carrier material for vitamins, a neutral or weak acidic pH

is required. The pH can be modified by subsequently treating the spray-dried silica with a base such as ammonia gas or by adjusting the pH of the re-suspended filter cake.

Determination of the pH of the silica is conducted on a 5% suspension of spray-dried silica according to the procedure of ISO 787-9.

The process of the present invention can be conducted under the condition that either the pH of the precipitation suspension is not modified after precipitation or the pH is lowered to 2–5, preferably 3, by adding acid, e.g. sulfuric acid.

The solid matter is separated from the suspension by known filtration methods such as a filter press (diaphragm filter press). The filter cake obtained in this way can be dried, for example by using a spin flash dryer. It is also possible to liquefy the filter cake by adding water and/or acid. If acid is employed, e.g. diluted sulfuric acid, a pH of <5, preferably 2–4, is adjusted in the suspension.

In a special embodiment of the process of the present invention, the product that has been subjected to a short retention drying process is subsequently treated with ammonia gas, or, alternatively, the drying process is conducted in the presence of ammonia gas.

Adding ammonia gas increases the pH of the silica and enables higher DBP absorption values.

A specified particle size distribution can be adjusted with the aid of a spray dryer or a jet dryer (jet tower). This can be adjusted by selecting the dryer type (single material jet, 2 material jet, gas/liquid jet, atomizing disk) and the spraying pressure. Typically a dryer with an atomizing disk is used.

Silicas of the present invention can be used as a carrier for converting liquids into powder form, e.g. in the crop protection, pesticide and animal feed industries, e.g. vitamin A and E,

choline chloride, as a free-flow or anti-caking agent, for example for table salt or instant meals, as well as in elastomers such as tires.

The silicas according to the present invention can be used to manufacture catalyst carriers.

Having now generally described this invention, a further understanding can be obtained by reference to certain specific examples which are provided herein for purposes of illustration only and are not intended to be limiting unless otherwise specified.

EXAMPLES

Reference Example 1

Precipitation of silica material is conducted as described in Example 1 of EP 0 078 909. For this purpose 60 m³ of water at a temperature of 40°C was added to a precipitation vessel, fitted with an EKATO MIG agitator and an additional EKATO shearing turbine. Commercially available water glass (26.8% SiO₂; 8.0 % Na₂O; density 1.346) and sulfuric acid (96%) flow into this vessel simultaneously at a speed of 10 m³/h and 0.9 m³/h respectively. After the 13th minute of precipitation the addition of water glass and acid is interrupted for 90 minutes. During this time both stirring devices continue to operate. From the 103rd minute the water glass and acid are added once more, at the above-mentioned rates, until the 146th minute. The solids content of the precipitation suspension is 47 g/l.

The solid of the suspension is removed by filtration in filter presses, washed and the resulting filter cake is liquefied under the effects of shearing. The solids content is 11.0%, the pH is 5. The silica suspension is then spray-dried. A DBP absorption value of 355 g/110 g was determined for the product that was obtained in the above manner.

The characteristics of the non-comminuted product are shown in the table below.

Reference Example 2

A precipitated silica was manufactured by the procedure described in Example 5 of EP 0 078 909. The procedure only differs from that of Reference Example 1 in the manufacture of the silica suspension for spray-drying. The filter cake is adjusted to a solids content of 16% by weight and a pH of 4.5 by adding water and acid under shearing conditions. The DBP absorption value is 349g/100 g.

The characteristics of the non-comminuted product are found in the table below.

Example 1

An amount of 60 m³ of water at a temperature of 38°C was added to a precipitation vessel, fitted with an EKATO MIG agitator and an additional EKATO disk agitator (350 mm diameter). While maintaining a pH of 6.5, commercially available water glass (27.1% SiO₂; 8.07% Na₂O; density 1.355) and sulfuric acid (96%) flow into this vessel simultaneously at a speed of 10 m³/h and 0.9 m³/h respectively. The acid is made to flow over the disk agitator, which is started when precipitation begins. After 13 minutes precipitation time, the addition of water glass and acid is interrupted for 90 minutes. During this time both the agitator and the EKATO disk agitator continue to operate. After this time the water glass and acid are added once more, at the above-mentioned rates and maintaining the above-mentioned pH for a further 34 minutes. The suspension is then acidified to pH 3 by adding sulfuric acid. The solids content of the precipitation suspension is 40 g/l. The suspension is subsequently filtered and washed in filter presses. For the further processing stage the filter cake is liquefied under shear with the addition

of water and small quantities of sulfuric acid. The pH is 5.0; the solids content is 12%. The silica suspension is then spray-dried. The free sulfuric acid in the material is neutralized downstream of the spray dryer with ammonia gas.

The characteristics of the non-comminuted product are found in the table below.

Example 2

A precipitated silica is manufactured as described above in Example 1, except that the filter cake obtained after processing in the diaphragm filter press is liquefied under shear with the addition of water and small quantities of sulfuric acid. The pH is 5.0 and the solids content is 11.0%. The silica suspension is then spray-dried.

Example 3

The precipitated silica is manufactured by the procedure of Example 1 above, except that the filter cake obtained after processing in the diaphragm filter press is liquefied upon the addition of water. The solids content is 8%.

The characteristics of the non-comminuted product are described in the table below.

Example 4

The precipitated silica is manufactured according to the procedure of Example 1 above, except that the filter cake obtained after processing in diaphragm filter presses with a solids content of 18% is dried for further processing in a spin flash dryer. (O.T. Kragh, Keramische Zeitschrift, Vol. 30, issue 7, pp 369–370, 1978; T. Hoepffner, Informations Chemie, Vol. 342, pp 141–145, 1992).

The characteristics of the non-comminuted product are shown in the table below.

Example 5

The precipitated silica is manufactured according to the procedure of Example 1 described above, except that the precipitation suspension is not acidified after precipitation is complete. The suspension is filtered in diaphragm filter presses and washed with highly diluted sulfuric acid with a pH of 1.6 to 1.8. For further processing the filter cake with a solids content of 18% is dried in a spin flash dryer. The free sulfuric acid contained in the material from the washing process is neutralized by adding ammonia, or, alternatively, the pH in the powder is raised to 7.7.

The characteristics of the non-comminuted product are shown in the table below.

Example 6

Manufacture of a precipitated silica and the subsequent processing of the suspension, including washing were conducted according to the procedure described in Example 4 above, except that for further processing the filter cake is liquefied by adding water under shear conditions. The pH is 3.2; the solids content is 11%. To neutralize the free sulfuric acid, the material is neutralized with ammonia gas downstream of the spray-dryer.

The characteristics of the non-comminuted product are shown in the table below.

TABLE

	Reference Examples		Examples										
	1	2	1	2	3	4	5					6	
pH	6.4	6.2	7.6	6.7	6.7	6.4	3.1	4.7	6.3	7.0	7.7	6.3	
DBP absorption g/100 g value	355	349	389	382	400	387	383	391	398	406	412	387	
Tapped density g/l	180	182	154	154	135	120	119	115	111	108	111	164	
ALPINE SR > 63µm %	10	23	15	1.4	1.8	0.3	0.2	0.3	0.3	0.2	0.1	18	
BET surface area m ² /g	429	515	454	458	485	484	501				476	495	
Suspension	~ 6		~ 3					~ 7					
Washing process	normal		normal					acidic					
Suspension of filter cake	5	4.5	5	5	5	N/A	N/A	(Filter cake has pH ~ 3)					3.2
Solids content %	11	16	12	11	8	18	18						11
NH ₃ addition	-	+	-	-	-	-	+	+	+	+	+	+	
Dryer	SP	SP	SP	SP	SF	SF	SF	SF	SF	SF	SF	SP	

* SF = Spin flash dryer
SP = Spray dryer

The disclosure of German priority Application No. 10058616.3 dated November 25, 2000 is hereby incorporated by reference into the present application.

Obviously, numerous modifications and variations of the present invention are possible in light of the above teachings. It is, therefore, to be understood that within the scope of the appended claims, the invention may be practiced otherwise than as specifically described herein.